

**METHANE de-NOX<sup>®</sup> for Utility PC Boilers**  
**Quarterly Technical Progress Report**  
**for the period ending March 31, 2005**

**Covering Period:** January 1 – March 31, 2005

**Principal Authors:** Bruce Bryan  
Joseph Rabovitser  
Serguei Nester  
Stan Wohadlo

**Date of Report:** April 28, 2005

**Award Number:** DE-FC26-00NT40752

**DOE Project Officer:**

Bruce Lani  
U.S. Department of Energy  
National Energy Technology Laboratory  
P.O. Box 10940, MS 922-273C  
Pittsburgh, PA 15236-0940

**Submitting Organization:**

Gas Technology Institute (GTI)  
1700 Mount Prospect Road  
Des Plaines, IL 60018-1804

**IGT Technical Contacts:**

Bruce Bryan  
(847) 768-0591  
[bruce.bryan@gastechnology.org](mailto:bruce.bryan@gastechnology.org)

Stan Wohadlo  
(847) 768-0594  
[stan.wohadlo@gastechnology.org](mailto:stan.wohadlo@gastechnology.org)

Joseph Rabovitser  
(847) 768-0548  
[Joseph.Rabovitser@gastechnology.org](mailto:Joseph.Rabovitser@gastechnology.org)

**Subcontractors:** Riley Power Inc. (RPI), a subsidiary of Babcock Power Inc., formerly  
Babcock Borsig Power.  
All-Russian Thermal Engineering Institute (VTI)

**DISCLAIMER**

This report was prepared as an account of work sponsored by an agency of the United States Government. Neither the United States Government nor any agency thereof, nor any of their employees, makes any warranty, express or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. Reference herein to any specific commercial product, process, or service by trade name, trademark, manufacturer, or otherwise does not necessarily constitute or imply its endorsement, recommendation, or favoring by the United States Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.

---

**ABSTRACT**

Large-scale combustion tests with caking bituminous coal was on hold this quarter mainly due to Riley's Commercial Burner Test Facility (CBTF) not having adequate weatherproofing to support operation under freezing conditions. The CBTF was secured and decommissioned for the winter season. CBTF bituminous coal tests shall continue to remain on hold now as a result of project funding limitations, however. No further modifications at the CBTF are planned until needed support is obtained. Activities this quarter have concentrated on finding additional support for the project. Currently, GTI has been granted a no-cost time extension through September 2005 and efforts to secure more support will continue in hopes that large-scale preheat caking bituminous combustion tests will be carried out as planned.

## TABLE OF CONTENTS

Disclaimer .....	2
Abstract .....	3
Table of Contents .....	4
Executive Summary .....	5
Experimental .....	6
Results and Discussion .....	8
Conclusions .....	9
References .....	9
Milestone Status Table.....	10

---

## EXECUTIVE SUMMARY

**Project Objectives:** The overall project objective is the development and validation of an innovative combustion system, based on a novel coal preheating concept prior to combustion, that can reduce NO<sub>x</sub> emissions to 0.15 lb/million Btu or less on utility pulverized coal (PC) boilers. This NO<sub>x</sub> reduction should be achieved without loss of boiler efficiency or operating stability, and at more than 25% lower levelized cost than state-of-the-art SCR technology. A further objective is to ready technology for full-scale commercial deployment to meet the market demand for NO<sub>x</sub> reduction technologies resulting from the EPA's NO<sub>x</sub> SIP call.

**Background:** A novel pulverized coal-preheating approach for NO<sub>x</sub> reduction was developed by the All Russian Thermal Engineering Institute (VTI) for use on PC utility boilers. The approach consists of a burner modification that preheats pulverized coal to elevated temperatures (up to 1500°F) prior to coal combustion. This releases coal volatiles, including fuel-bound nitrogen compounds, into a reducing environment, which converts the coal-derived nitrogen compounds to molecular N<sub>2</sub>. The quantity of natural gas fuel required for PC preheating is in the range of 3 to 5% of the total burner heat input. Basic combustion research and development of the preheat PC burner was conducted by VTI in the early 1980's. Following these promising laboratory results, commercial-scale PC preheating burners of 30 and 60 MW<sub>t</sub> capacity were developed and demonstrated in field tests conducted in several Russian power stations.

The advanced PC preheating combustion system being developed in this project for direct-fired PC boilers combines the modified VTI preheat burner approach with elements of IGT's successful METHANE de-NOX technology for NO<sub>x</sub> reduction in stoker boilers. The new PC preheating system combines several NO<sub>x</sub> reduction strategies into an integrated system, including a novel PC burner design using natural gas-fired coal preheating, and internal and external combustion staging in the primary and secondary combustion zones.

Design, installation, shakedown and initial PRB coal testing of a 3-million Btu/h pilot system at RPI's Pilot-Scale Combustion Facility (PSCF) in Worcester, MA demonstrated that the PC Preheat process has a significant effect on final NO<sub>x</sub> formation in the coal burner. Modifications to both the pilot system gas-fired combustor and the PC burner led to NO<sub>x</sub> reduction with PRB coal to levels below 100 ppmv with CO in the range of 35-112 ppmv without any furnace air staging. Pilot testing with PRB coal is complete.

Initial pilot testing with caking coal resulted in deposition and plugging by caked material inside of the gas combustor. A series of modifications to the combustor configuration and operation have been developed and tested during previous quarters, and testing of several more versions was continued in the current quarter. One of these approaches using a stainless steel liner indirectly cooled with air was successful in sustaining operation with caking coal up to 150 lb/h.

Installation and shakedown testing with natural gas and PRB coal was completed for the large-scale prototype coal preheater. Large-scale testing with PRB coal was discontinued due to the inability of the coal mill to meet the 85 MMBtu/h design firing rate. The project was therefore redirected toward design, installation and testing of the 85-million Btu/h preheater for bituminous coal. Based on extensive pilot-scale testing completed earlier in the project, 2-D modeling and design activities were then completed based on the use of staged, annular protective air films to control temperature and prevent deposition on the preheater walls.

Riley burner design engineers with guidance from GTI completed a preliminary mechanical design for a bituminous coal preheater. The design basis came from CFD studies conducted by GTI; materials of construction and thermal growth considerations were finalized by Riley staff. The bituminous preheat burner consists of a multi-barrel burner coal pipe; each barrel larger in diameter than the next which facilitates implementation of an air layer on the inside surface of each barrel wall. The air layer is critical in preventing the formation and buildup of coal agglomeration on the interior barrel walls.

With the burner design complete, preparations for retrofitting Riley's CBTF would have normally begun. These preparations are on hold, however, because of weather constraints as well as funding limitations. Because the CBTF construction was not properly weatherproofed to permit reliable operation in freezing conditions testing was put on hold over the winter season. Then, an evaluation of funds available showed that further support was needed before test preparation work and combustion tests proceeded. GTI was granted a no cost time extension in hope of securing additional support of this research.

## **EXPERIMENTAL**

### Pilot Unit

Fabrication, installation and initial testing of the pilot-scale coal preheating system were completed in the fall of 2001. The unit is sized for operation with natural gas and pulverized coal at a total firing rate of approximately 3-million Btu/h and includes all equipment and controls necessary to operate and monitor energy and environmental performance of the system. A gravimetric feeder is used to regulate pulverized coal flow through a rotary airlock into a natural gas-fired preheater combustor. The combustor produces hot combustion gases, which combine with the pulverized coal to produce a mixture of coal char and pyrolysis products at the desired test temperature.

In the original pilot system configuration, the combustor centerline was vertical and two pipe sections after the combustor provided additional residence time for the coal at the preheated conditions prior to entering the PC burner. However, pilot testing experience together with commercial design guidance from RPI redirected the development of both the pilot and commercial units toward a horizontal combustor design with no diameter change between the combustor and burner. The preheater combustor was therefore relocated to a horizontal configuration with the combustor exit coupled directly to the PC burner inlet, eliminating the two pipe sections.

In the modified pilot unit, the velocity of the devolatilization products in the combustor and burner is increased over previous pilot testing to minimize separation and impingement of coal on inner surfaces prior to reaching the burner face. The higher velocities are more consistent with standard design criteria developed by RPI for their commercial CCV burners. The higher combustor velocities were achieved by inserting a liner in the combustor to reduce its internal diameter. The liner also facilitates testing of various designs and operating approaches to eliminate plugging of the combustor with caking coals. Various liner materials, including metal and ceramic, and liner cooling methods are being developed and tested to determine their effect on wall deposition and plugging.

During testing, real time operating data are collected at 1-second intervals and recorded by the personal computer-based data acquisition system (DAS). The concentrations of CO, CO<sub>2</sub>, O<sub>2</sub>, THC and NO/NO<sub>x</sub> in the pilot unit exhaust and the furnace exit are continuously monitored by on-line gas analyzers, including a Rosemount Analytical Model 880A infrared CO analyzer, a Rosemount Analytical Model 880A infrared CO<sub>2</sub> analyzer, a Rosemount Model 400 flame ionization total hydrocarbons (THC) analyzer, a Rosemount Analytical Model 755R paramagnetic O<sub>2</sub> analyzer, and a ThermoElectron Model 14A chemiluminescence NO<sub>x</sub> analyzer.

The preheater gas combustor temperatures are monitored by thermocouples installed on both the outer walls and inside of the combustion chamber. Temperature of the gas/air mixture is monitored in the gas/air plenum entering the combustor nozzles.

### Large-Scale Prototype Unit

The CBTF comprises a large horizontally fired dry bottom furnace capable of testing full-scale burner systems with firing capacities up to 100 MMBtu/h. The furnace is fully integrated with coal storage, grinding and feeding, emissions control, and continuous flue gas sampling and analytical subsystems.

Coal is pulverized and dried in a DB Riley Model 350 Atrita pulverizer, which is fed from a 40-ton bunker by a weigh-belt feeder and rotary valve. The mill's air supply system includes a Venturi air flow meter, fan and natural gas direct-fired heater to supply a measured amount of hot air to the pulverizer to dry and transport the coal. The CBTF is capable of firing in both the direct fire mode and from an intermediate storage bin (indirect fire). All testing will be conducted in the direct fire mode to simulate the most common firing method in the U.S market. Drying and transport air will be separated from coal stream immediately ahead of the preheater combustor inlet. The separated air will be directed to one of the three air channels in the coal burner. Secondary air will be preheated to 600 °F by a separate fan and heater and routed to the coal burner. Air can be routed to the burner through an integral windbox plenum or through separate external ducts. Flow to each burner air channel can be regulated independently. Ports are also available at several locations for furnace air staging.

Flue gas composition will be monitored continuously. A multiple-probe sampling grid consisting of sintered Hasteloy filters is mounted in the CBTF exit duct, just upstream of the flue gas scrubber. The in-duct filters remove the majority of particulate, and the flue gas is drawn through stainless steel tubing, ice-bath conditioners, and a final filter by individual sample pumps. A rotameter at the outlet of each pump is used to admit equal flow of clean, dry sample from each grid probe to a manifold. The proper flow of sample for each continuous analyzer is supplied from the manifold.

Continuous monitors are used to measure O<sub>2</sub>, CO<sub>2</sub>, CO, NO/NO<sub>x</sub> and SO<sub>2</sub>. In addition to the gas sampling grid, a separate water-cooled probe is used to withdraw particulate samples at the CBTF outlet for determination of carbon burnout. A high velocity thermocouple probe monitors furnace outlet temperature.

The CBTF is fully instrumented to allow continuous measurement and recording of all relevant flow, pressure and temperature readings to allow complete material and energy balances to be developed for each testing period.

---

## RESULTS AND DISCUSSION

### **Project Status:**

#### *Task 1.1 Pilot-Scale Design*

No work was performed on this task during the reporting period.

#### *Task 1.2 CFD Modeling*

##### Pilot Unit

No work was performed on this task during the reporting period.

##### Large-Scale Prototype Unit

No work was performed on this task during the reporting period.

#### *Task 1.3 Pilot-Scale Equipment Fabrication and Installation*

No work was performed on this task during the reporting period.

#### *Task 1.4 Pilot-Scale Testing*

No work was performed on this task during the reporting period.

#### *Task 1.5 Pilot-Scale Data Evaluation*

No work was performed on this task during the reporting period.

#### *Task 2.1 Commercial Prototype Engineering Design*

No work was performed on this task during the reporting period.

#### *Task 2.2 Baseline Data Review*

No work was performed on this task during the reporting period.

#### *Task 2.3 Commercial Prototype Construction*

No work was performed on this task during the reporting period.

#### *Task 2.4 Commercial Prototype Testing*

No work was performed on this task during the reporting period.

#### *Task 2.5 Data Processing and Evaluation*

No Work was performed on this task during the reporting period.

#### *Task 2.6 Commercialization Plan Development*

This task has been deleted from the project workscope.

#### *Task 2.7 Design and Fabrication of Commercial Burner System*

This task has been deleted from the project workscope.



---

*Tasks 1.6 & 2.8 Management and Reporting*

An evaluation of project schedule and costs showed insufficient time and funding to successfully conduct large-scale preheat combustion tests with caking bituminous coal. Work at Riley's CBTF was stopped and installation and testing of the 85 MMBtu/h bituminous coal preheating system is on hold until additional support is obtained. A request for a no-cost time extension was received from DOE, which extends the project through September 2005. Efforts to secure additional funding and or determining the best path forward is underway. A phone contact with ALSTOM Power was made exploring future cooperation and interest. Further inquiries with other boiler manufacturers are planned.

**Plans for Next Quarter:**

Continue efforts to secure a path forward; find additional project funding from cost share sources sufficient to retrofit the CBTF and conduct preheat caking bituminous coal combustion tests.

**CONCLUSIONS**

Project activities at the CBTF site have been placed on hold dependent on acquiring additional funds to complete large-scale bituminous coal testing and development work.

**REFERENCES**

N/A

**Milestone Status Table:** The proposed revised completion dates for all project tasks and major milestones are shown below.

ID No.	Task / Milestone Description	Planned Completion	Actual Completion	Comments
◆	Kickoff Meeting	5/2/2000	5/2/2000	Complete
1.0	Technology Development			
1.1	Pilot-Scale Design	8/31/2000	12/31/2000	Complete
1.2	CFD Modeling-Pilot and Commercial Scale	6/30/2001		Pilot-scale modeling complete
1.3	Pilot-Scale Equipment Fabrication and Installation	11/30/2000	9/30/2001	Pilot Scale complete
1.4	Pilot-Scale Testing – Caking Coal	6/15/2004		Complete
1.5	Pilot-Scale Data Evaluation – Caking Coal	6/15/2004		Complete
1.6	Task 1 Management and Reporting	7/15/2004		
◆	Task 1 Report	8/15/2004		Hold
2.0	Technology Validation			
2.1a	Commercial Prototype Engineering Design - PRB Coal	4/15/2004	6/30/2004	Complete
2.1b	Commercial Prototype Engineering Design - Caking Coal	8/30/2004		
2.2	Baseline Data Review	4/15/2004	4/15/2004	Complete
2.3a	Commercial Prototype Construction - PRB Coal	4/15/2004	6/15/2004	Complete
2.3b	Commercial Prototype Construction - Caking Coal	9/30/2004		Hold
2.4a	Commercial Prototype Testing - PRB Coal	6/30/2004	8/30/2004	Discontinued
2.4b	Commercial Prototype Testing - Caking Coal	11/30/2004		New Date: Unresolved
2.5a	Data Processing and Evaluation - PRB Coal	7/30/2004	8/30/2004	Complete
2.5b	Data Processing and Evaluation - Caking Coal	7/31/2004		
2.6	Commercialization Plan Development	--	--	Task Eliminated
2.7	Design and Fabrication of Commercial Burner System	--	--	Task Eliminated
2.8	Task 2 Management and Reporting	9/30/2005		
◆	Final Report	9/30/2005		New Date: 12/31/2005